



2004 DOE Hydrogen, Fuel Cells, & Infrastructure Technologies Program Review

Development of Polybenzimidazole-based, High Temperature Membrane and Electrode Assemblies for Stationary and Automotive Applications

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Contains no proprietary or confidential information.

PROJECT OVERVIEW AND OBJECTIVES TO DATE

To identify and demonstrate an MEA based on a high-temperature polybenzimidazole (PBI) membrane that can achieve the performance, durability, and cost targets required for both stationary and automotive fuel cell applications.

- ❖ Complete initial screening of potential PBI-based chemistries and structures and downselect top 5 - 10 candidate materials based on chemical and physical properties.
- ❖ Initiate rapid screening of candidate PBI materials in 50 cm² MEAs.
- ❖ Initiate detailed electrochemical characterization of MEAs made with selected PBI polymers.
- ❖ Initiate evaluation of low cost acid-absorbing materials for phosphoric acid management within the system.
- ❖ Initiate design and development of bipolar plates with PBI-specific flow fields.
- ❖ Initiate development of a PBI membrane-based MEA with advanced electrode structures providing high catalyst utilization and performance exceeding that of Nafion.

DOE TECHNICAL BARRIERS

- ❖ O. Stack Material and Manufacturing Cost
- ❖ P. Durability

DOE TECHNICAL TARGETS

- ❖ Applicable to both automotive and stationary fuel cell systems
- ❖ Operating temperature $> 120^{\circ}\text{C}$
- ❖ Operating pressure from 1 – 3 atm (abs)
- ❖ Membrane area specific resistance $< 0.1 \Omega\text{-cm}^2$
- ❖ Gas crossover $< 1\%$
- ❖ MEA manufacturing process scalable from 50 to at least 250 cm^2
- ❖ Automotive MEA cost target of $< \$10/\text{kW}$ at a volume of 500,000 fuel cell stacks per year
- ❖ Stationary system cost target of $< \$1500/\text{kW}$ at 1,000 fuel cell stacks per year
- ❖ Projected design lifetime $> 40,000$ hours

TEAM

- ❖ Plug Power Inc.
 - Prime contractor
 - Membrane and membrane electrode assembly (MEA) characterization
 - PBI-specific hardware development
- ❖ Rensselaer Polytechnic Institute
 - Membrane formulation, evaluation, and selection
 - Membrane processing parameter optimization
- ❖ Albany NanoTech, University at Albany, SUNY
 - Nanofabricated electrodes
- ❖ Celanese Ventures GmbH
 - Membrane and MEA production
 - MEA cost modeling

PROGRAM BUDGET

CY		Total \$		DOE \$		Contractor \$
2003 Actual	\$	509,578	\$	407,662	\$	101,916
2004	\$	3,352,106	\$	2,681,685	\$	670,421
2005	\$	2,268,780	\$	1,815,024	\$	453,756
2006	\$	1,163,799	\$	931,039	\$	232,760
Total	\$	7,294,263	\$	5,835,410	\$	1,458,853

CY 2003 shortfall of \$600K moved to 2004 - 06.

APPROACH - Focus 1

Screening of candidate polymers and membrane fabrication processes

- ❖ Task 1: Polymer screening and preliminary evaluation
 - Identify and standardize chemical, physical, and mechanical test methods
 - Identify potential PBI-based polymers for evaluation
 - Characterize polymers by molecular weight, phosphoric acid content, proton conductivity, and film mechanical strength
 - Identify 5 - 10 lead candidate materials for further evaluation
- ❖ Task 2: Detailed polymer characterization
 - Characterize the structure and properties of polymer films
 - Determine the relationships between polymer structure and membrane properties
 - Develop processes to produce larger quantities of material (~1 L)
 - Identify 1 - 3 candidates for continued evaluation
- ❖ Task 3: Low-cost membrane formation techniques
 - Identify the key parameters for membrane formation
 - Define the optimum processing conditions for membrane formation (e.g., polymer concentration, temperature, casting speed, humidity levels)
- ❖ Task 4: Membrane scale-up
 - Demonstrate ability to produce membranes in sufficient quantities to meet program needs.

APPROACH - Focus 2

MEA Characterization

- ❖ Task 5: 10-50 cm² MEA screening
 - Fabricate MEAs from membranes made from candidate and standard gas diffusion layers
 - Test at limited conditions - 120°C and 160°C, reformat with 50 ppm CO and 10,000 ppm CO
 - Operate for 10 hours
 - Combine MEA screening performance with Task 1 property screening data for downselection
- ❖ Task 6: 50 cm² MEA evaluation
 - Conducted detailed parametric studies of MEAs made with membranes with acceptable physical and electrochemical properties
 - Operate cells at multiple temperatures between 100 and 200°C, pressures between 1 and 3 atm (abs), hydrogen/air and reformat/air, multiple CO concentrations in reformat.
 - Combine MEA performance data with property data obtained in Task 2 for selection of final candidate materials.
- ❖ Task 7: 440 cm² MEA test in short stack
 - Evaluate the final membrane material(s) in short stack
- ❖ Task 8: Long-term MEA performance characterization
 - Fabricate MEAs for testing in a 50 cm² single cell, in a 440 cm² single cell, and in a 440 cm² short stack
 - Operate cells/stack for at least 1,000 hours under expected operating conditions
 - Determine cell degradation rate and degradation mechanism

APPROACH - Focus 3

Hardware Development and Demonstration

❖ Task 9: Acid management

- Characterize the acid-absorbing capacity of several candidate materials under different temperature and pressure conditions.
- Select the optimum material and design an enclosure with at least two-years of acid-absorbing capacity.

❖ Task 10: PBI-specific flow field design

- Conduct CFD simulations to determine the optimum flow field geometry for PBI membranes
- Confirm simulation results with 50 cm² cells
- Design prototypical sized plates incorporating lessons learned
- Design sealing mechanism that provides adequate sealing with minimal compression.

❖ Task 11: Electrode development and performance improvement

- Develop a model of phosphoric acid electrodes to determine optimum electrode properties
- Characterize the effects of electrode structure on performance.
- Develop a nanostructured electrode that maximizes catalyst utilization.

❖ Task 12: Cost assessment

- Build a cost projection model that incorporates data obtained during this program - membrane composition, membrane and MEA manufacturing processes, MEA performance, degradation rates, etc.
- Project MEA costs based on anticipated market demand

SCHEDULE / MILESTONES

FOCUS 1 (8/03 - 6/06)

1

2

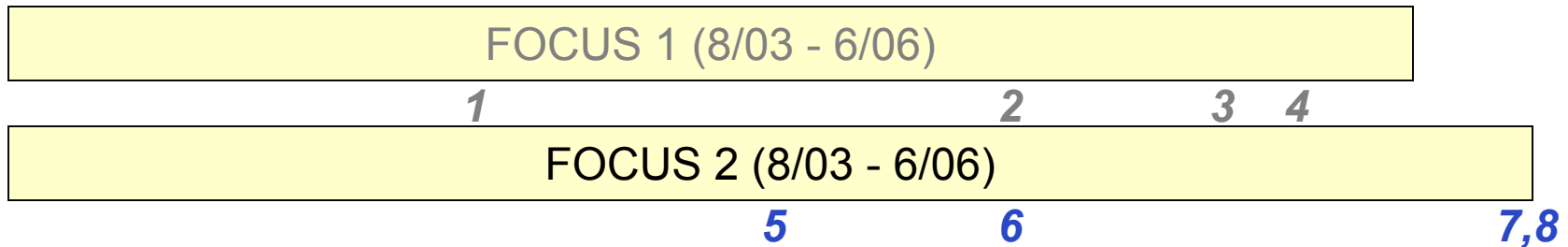
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Focus 1 - Polymer and membrane screening and fabrication

- 1 *Initial list of 5 - 10 candidate materials*
- 2 *List of ~3 final candidate materials*
- 3 *Membrane fabrication process parameters defined*
- 4 *Full-size MEAs from scaled up process delivered for testing*

SCHEDULE / MILESTONES



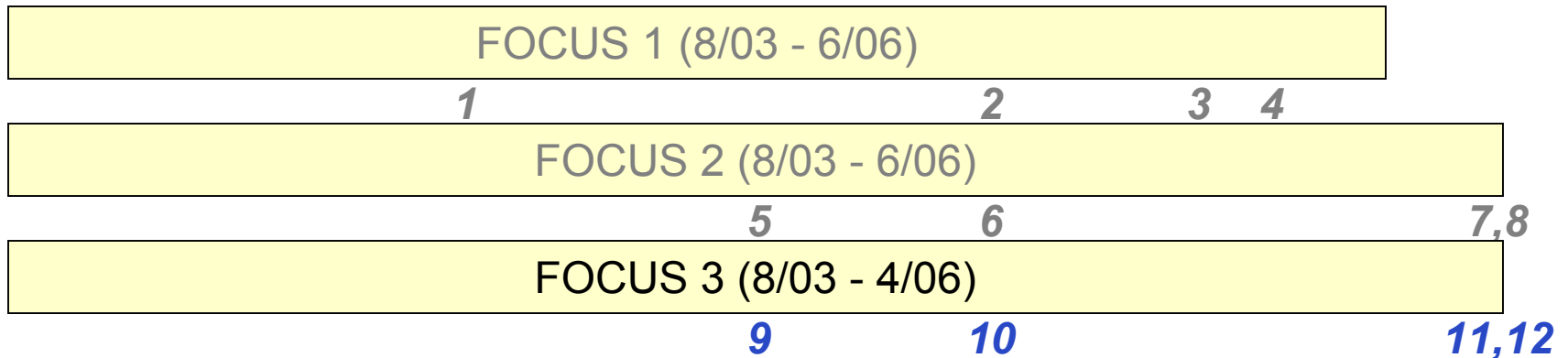
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- 4 *Full-size MEAs from scaled up process delivered for testing*

Focus 2 - MEA characterization

- 5 *Initial MEA screening complete*
- 6 *MEA electrochemical property data*
- 7 *Full-sized MEA testing in short stack completed*
- 8 *MEA degradation mechanism(s) and rate identified*

SCHEDULE / MILESTONES



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Focus 3 - Hardware development and demonstration

- 9 Absorbent material and enclosure for acid management verified
- 10 Optimized flow field designed and verified
- 11 Improved electrodes demonstrated
- 12 MEA cost model and cost projections completed

PROJECT SAFETY

- ❖ Full-time EHS manager provides oversight, training, and guidance.
- ❖ Annual laboratory safety training of all personnel and new employees.
- ❖ Laboratories designed to meet OSHA/NFPA Class I, Div. 2 requirements.
- ❖ Standard operating procedures prepared and maintained for all test and laboratory equipment.
- ❖ Safety reviews of all test systems and laboratories prior to operation.
- ❖ Chemical inventory and storage records audited annually.
- ❖ Use of an Open Safety Items tracking system to schedule and ensure closure of any identified safety issue.
- ❖ All products subjected to industry certifications as appropriate (e.g., UL, CSA, NEBS, and CE).

TECHNICAL ACCOMPLISHMENTS

Polymer Screening (Task 1)

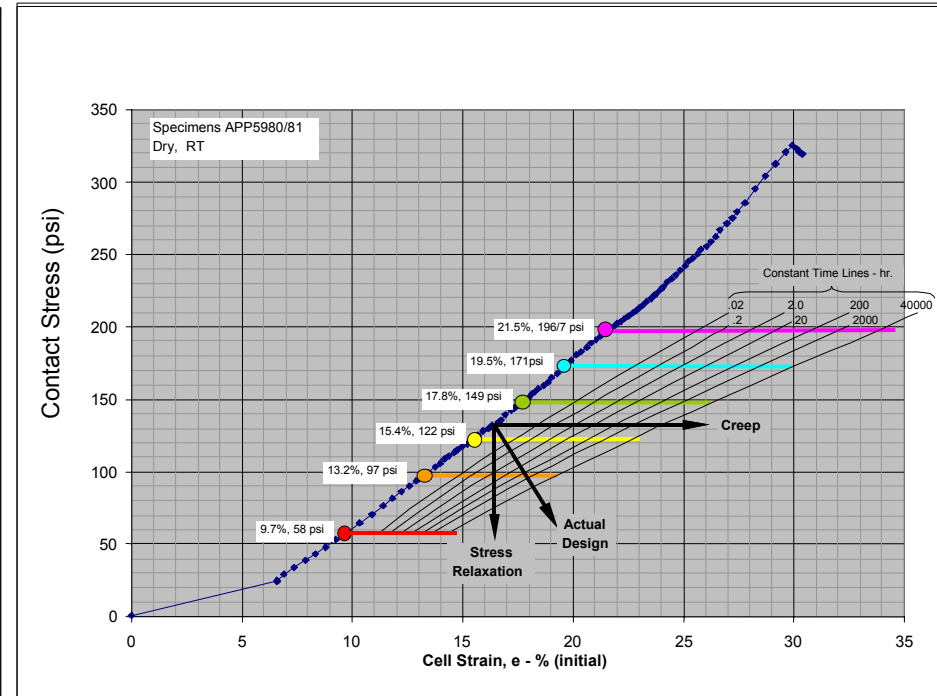
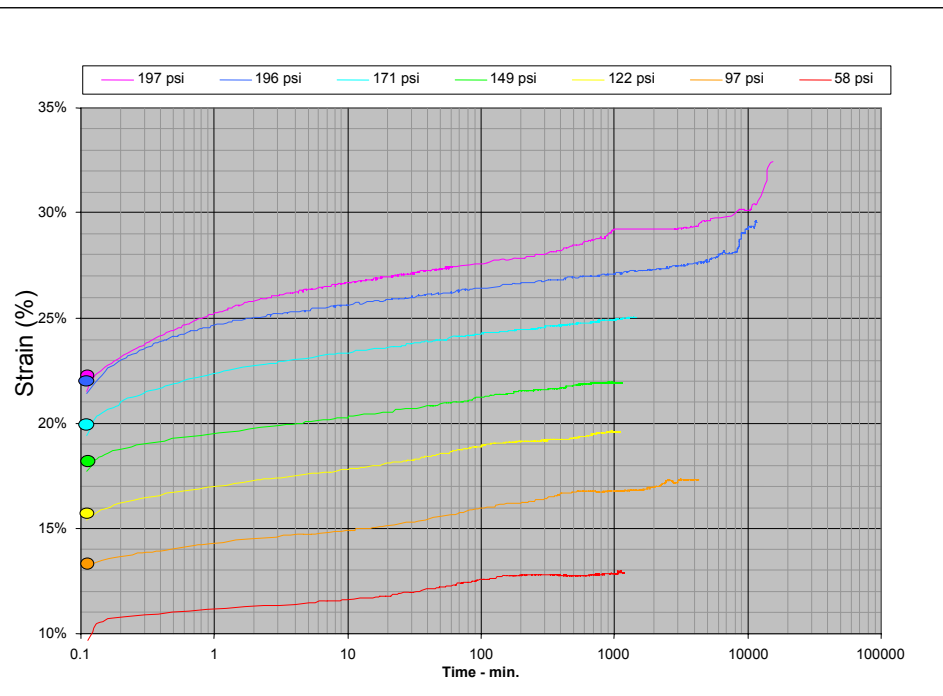
Composition	IV (dL/g)	Polymer Content (wt%)	Acid Content (wt%)	Water Content (wt%)	n(H ₃ PO ₄)/n(PBI)	Conductivity (S/cm) at 160° C
1	2.9	6	65	30	38	0.18
2	4.1	4	72	24	49	0.18
3	0.8	15	60	25	46	0.2 (*)
4	1.7	6	80	14	42	0.2 (*)
5	1.2	21	63	16	10	0.1

(*) Measured at 140°C; membrane melted at 160°C.

- First 5 PBI compositions identified, each with a unique chemical structure.
- Membranes were made from each of the first 5 polymers.
- High molecular weight polymers were obtained (typical plant-grade PBI inherent viscosity is 0.8 - 1.0 dL/g).
- All of the phosphoric acid contents obtained were greater than previously reported for PBI materials.

TECHNICAL ACCOMPLISHMENTS

Membrane Characterization (Task 2)

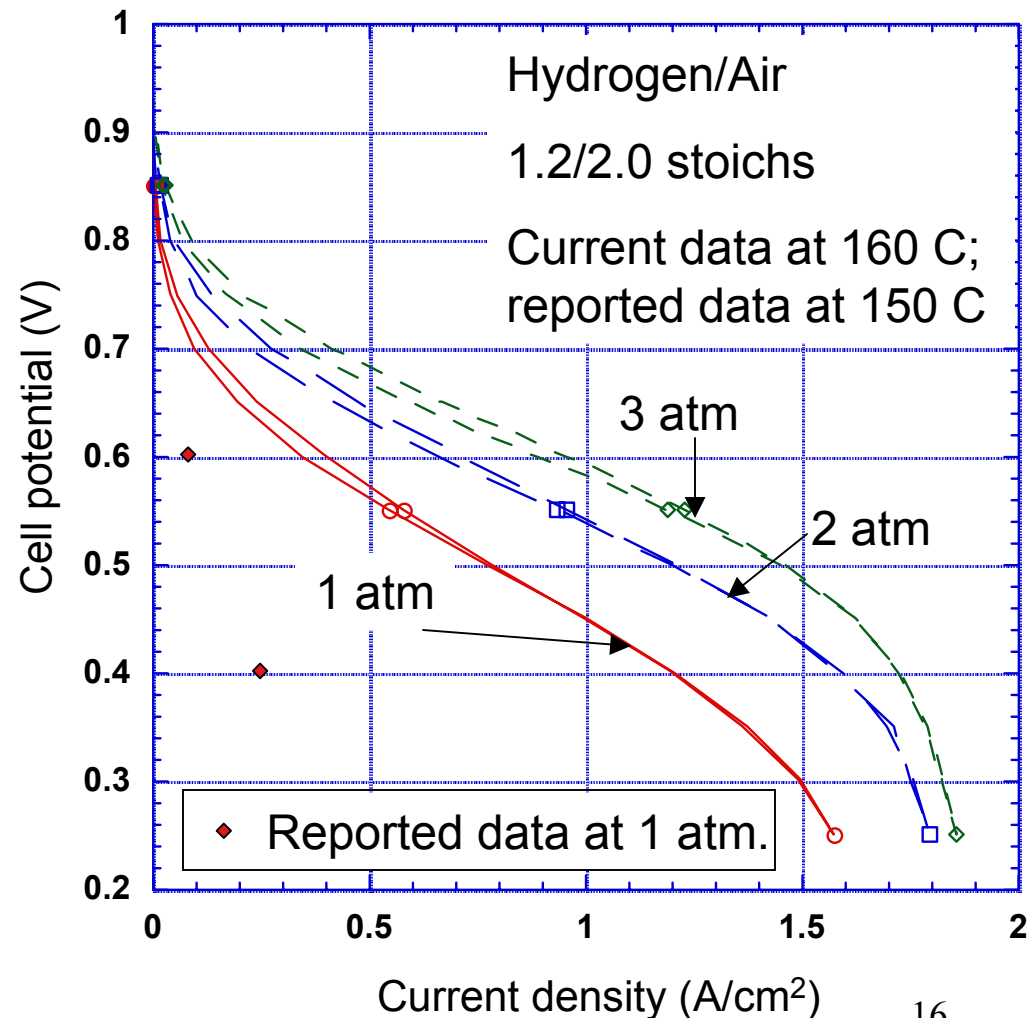


- ❖ Membranes exhibit a high initial rate of creep under constant load.
- ❖ This behavior has significant ramifications for stack design.
- ❖ Membrane behavior will affect the design of stack seals, end hardware, and plates.

TECHNICAL ACCOMPLISHMENTS

MEA Screening (Task 5)

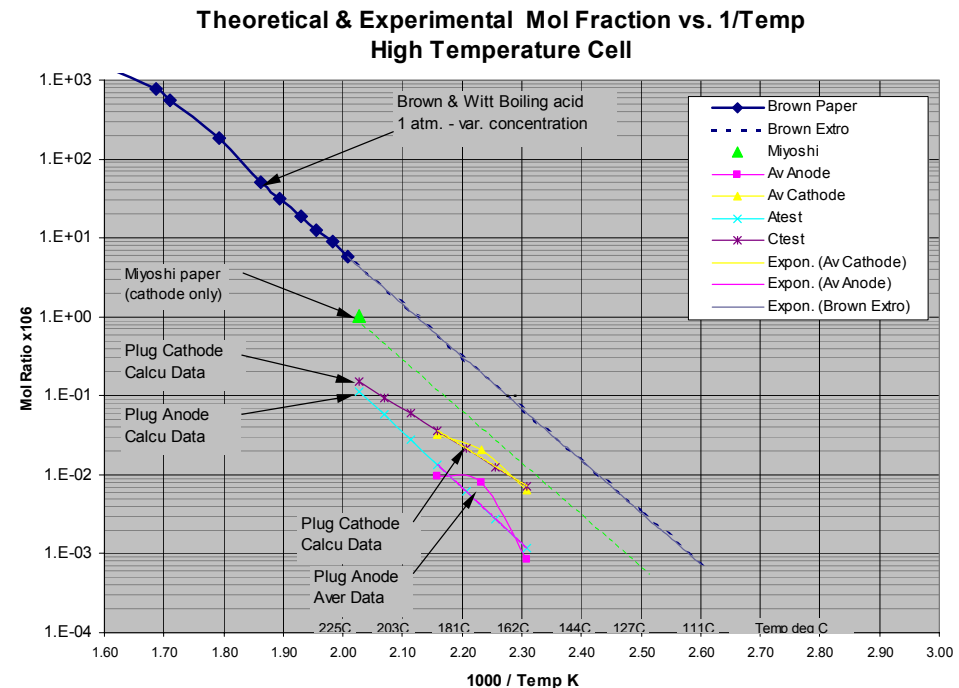
- MEA performance exceeds previously reported polarization data.
- Measured pressure effect:
 $\Delta V \text{ (mV)} = 75 \log(P_2/P_1)$
- PAFC theoretical value:
 $\Delta V \text{ (mV)} = 146 \log(P_2/P_1)$



TECHNICAL ACCOMPLISHMENTS

Acid Management (Task 9)

- ❖ Identified the mechanisms for acid transport in and from a cell:
 - ❖ Diffusion
 - ❖ Capillary transport
 - ❖ Compression
 - ❖ Evaporation
- ❖ Steady state phosphoric acid evaporation losses were studied on the current membrane and found to be less than theoretical.
- ❖ Isolating a cell from test station prevents phosphoric acid loss during startup and shutdown .

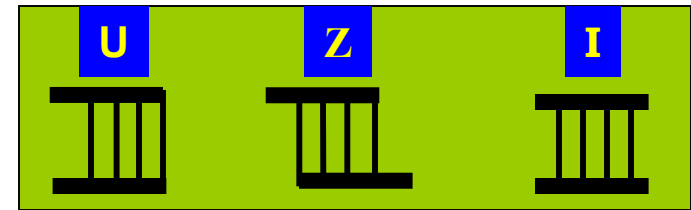


*Projected cell life is 40,000 hours
with these loss rates.*

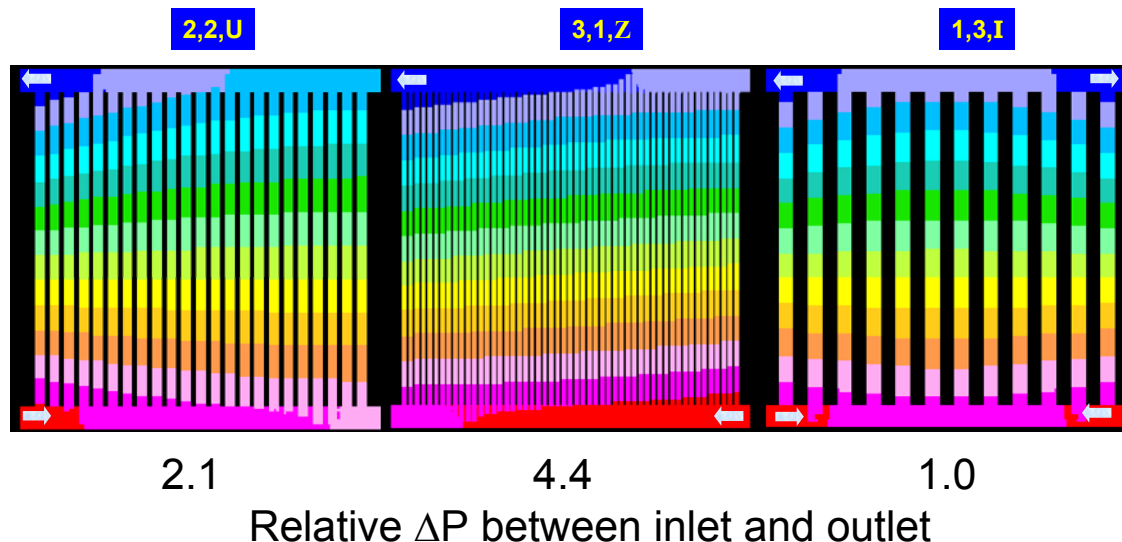
TECHNICAL ACCOMPLISHMENTS

Flow Field Optimization (Task 10)

Experiment number	Channel/land ratio	Relative channel width	Relative flow area	Manifold configuration
1	1.0	1.0	1.0	U
2	1.0	2.0	2.0	Z
3	1.0	3.0	3.0	I
4	2.0	1.0	2.0	I
5	2.0	2.0	3.0	U
6	2.0	3.0	1.0	Z
7	3.0	1.0	3.0	Z
8	3.0	2.0	1.0	I
9	3.0	3.0	2.0	U



Pressure distribution - Relative flow area = 3.0



- ❖ Flow uniformity decreases as flow area increases.
- ❖ Channel width does not impact flow distribution.
- ❖ Channel-to-land ratio does not impact flow distribution.
- ❖ Manifold size and configuration strongly impact flow uniformity and pressure distribution.

KNOWLEDGE AND TECHNOLOGY TRANSFER ACTIVITIES

- ❖ Elter, John, “IPHE as Facilitator of Hydrogen and Fuel Cell Markets for Stationary Applications,” Presentation to the International Partnership for a Hydrogen Economy, Washington, DC, November 2003.
- ❖ “NextGenCell - The next generation of stationary fuel cells,” Expression of Interest submitted to the European Commission, Plug Power Inc., Vaillant GmbH, and Celanese Ventures GmbH, March 2004.
- ❖ Benicewicz, Brian, “PBI Membranes and MEAs for Stationary and Automotive Applications,” Presentation to Los Alamos National Laboratory, Los Alamos, New Mexico, March 2004.
- ❖ Benicewicz, Brian, “PBI Membranes and MEAs for Stationary and Automotive Applications,” Presentation to University of New Mexico, Albuquerque, New Mexico, March 2004.

FUTURE WORK

❖ Remainder of 2004:

- Prepare additional polymers and membrane materials for testing.
- Test and evaluate lead candidate materials in 50 cm² single cells.
- Characterize the physical and mechanical properties of the lead candidate materials.
- Develop a concept to manage acid loss.
- Design a prototypical size PBI-specific flow field.

FUTURE WORK

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- Develop a concept to manage acid loss.
- Design a prototypical size PBI-specific flow field.

❖ 2005 - 2006:

- Downselect to the 1 - 3 polymers that show highest likelihood of achieving the program performance, reliability, and cost goals.
- Complete an in-depth parametric characterization of final candidate materials.
- Complete and verify an optimized flow field design in a short stack.
- Complete and demonstrate appropriate acid management hardware.
- Determine and understand the MEA degradation rate in a short stack.
- Demonstrate a PBI-based MEA that meets or exceeds program goals in a short stack.
- Develop and exercise a model to project MEA cost at high volumes.



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